## Continuous SSF Experiments with Tammy Kay Hayward June 16, 1995

Corn Fiber

Experiment Run Dates: January 31-March 17th 1995
Researchers: Tammy Kay Hayward and Kevin M. Connors
Oral Presentation: Amoco-NREL TSC March 1995 (tkh)

Amoco CRADA Bench Scale Research Director: Christos Hatzis

Continuous SSF System Director: George Philippidis

Lab Book Reference: 1651 001-007.

<u>Objectives</u>: To establish a continuous SSF steady state using Corn Fiber and collect data. Experiment represents the first attempt to use a non-hardwood feedstock in the system. To test the effect of dilution rate and enzyme loading on ethanol yield in continuous mode.

### Materials and Methods:

Method of Operation: There were two feed vessels, the first one contained the and CSL in a pump race, the second feed vessel contained amylase and cellulase enzymes. The yeast maintained their population in the New Brunswick Bioflo III reactor at the set dilution rates. Addition of feeds were coordinated by the same timer on a pulse feed basis. Fermentation product flowed out of the system via a 1/2" port in the side of the reactor. This overflow port insured a constant reactor volume of 1.2 liters. The spent slurry was collected in a sterile container and its weight was displayed by a Ohaus balance and recorded at the time of sampling. See Figure 1 "Schematic of the Continuous System". Whole slurry samples were removed via bottom sample port on the reactor. Sterile air was introduced in the head space of the vessel in order to provide enough gas to meet the minimum flow requirements of the mass spectrometer. The off gas was analyzed by the Fisons VG Prima 600 mass spectrometer for carbon dioxide. This CO2 measurement is one of the best ways to assess the health of the fermentation and prevent wash out. Rotometers monitored the flow of air and off-gas, the Bioflow's flow controller served to hold the flow constant.

Residence Times: A test run using the com fiber solution was conducted to determine the amount of slurry per discharge and calibrate the timer accordingly. Actual slurry discharge time was fixed at 0.4 seconds throughout the run. Flow is controlled by varying the rest time interval (how long between discharges). See Figure 2 "Tests on Delivery" Enzyme feed was also controlled by the timer. Discharge time remained fixed at 9 seconds throughout the run. Enzyme flow was controlled by adjusting the speed of the enzyme pump. Each time the enzyme loading was changed, the pump was isolated and tested by measuring the volume in microliters per 9 second discharge. The speed was fine tuned until the desired volume was obtained. For the first dilution rate the master timer was set to discharge every 36 minutes. The goal was a 3 day residence time. Three days was the longest residence time the PDU could currently operate at. The second dilution rate was set to discharge every 24 minutes. The residence time was shortened to 2 days. The overflow balance is used to determine the actual through put of the system. The overflow method accounts for clogs, mechanical failures and other disturbances to the system.

Corn Fiber: The substrate used in this experiment was the corn fiber sent to NREL by AMOCO in December of 1994. Material from bucket #11 was stirred and then diluted in D.I. water to form a final feed concentration of 40 w/w %. This was the maximum

concentration that the magnetic stir bar in the feed vessel would tolerate. The solution was neutralized with lime to pH 5. Overliming was not performed. CSL was added to the feed and then the ECF and CSL mixture was autoclaved for 30 minutes.

CSL: The nutrient source employed was 1% v/v Grain Products Corporation Corn Steep Liquor. This CSL is a very thick mixture containing solids. Filter sterilization of the raw CSL proved difficult. So, a 10% dilution of the CSL in DI water was adjusted to pH 5 with ammonium hydroxide, and autoclaved for 30 minutes. This autoclaved stock solution was then filter sterilized and added to the feed flasks prior to autoclaving.

Cellulase and Amylase: The PDU lot of CPN was used as the cellulase enzyme. The activity of the pure, sterile filtered, cellulase was measured by Bill Adney and determined to be 70 FPU per mL. The glucoamylase was a A. niger preparation from Sigma. The activity of the sterile filtered, enzyme as stated on the bottle is 6100 units per mL. The amylase enzyme is suspended in one molar glucose and the cellulase enzyme is in 300 g/L sucrose, both have ramifications on the ethanol yield. The two enzymes were mixed together in the enzyme reservoir to achieve a 10 FPU to 100 amylase unit ratio. The recipe was 102.9 mL CPN cellulase and 3.9 mL of Sigma amylase. Enzyme loadings were based on the composition of the co

Yeast: The organism used in this experiment was from a plate given to NREL by Ray Bigelis (AMOCO) in December of 1994. A freeze back of this culture was performed. The vials were stored in the new -75 C freezer. A two stage YPD (1% yeast extract. 2% peptone. 2% dextrose) inoculum grown at 34°C was prepared from a vial of the parent strain Labatt 1400. A 10% v/v inoculum was then used to start the batch SSF. No adaptation to the pretreated corn fiber was performed. The yeast maintained its population in continuous mode.

SSF Conditions: The SSF was run at 34°C. 150 rpm, 40 w/w% ECF, with 1% v/v CSL at pH 5 with cellulase and amylase enzymes and head space air. com fiber, CSL and enzymes were added on a semi-continuous basis and spent slurry containing ethanol was removed by gravity on a constant basis.

### Experimental Design:

- 1. Establish Steady State with ECF, 3 day residence time, 10 FPU/100 units
- 2. Decrease residence time to 2 days
- 3. Double the enzyme loading (20 FPU/200 units)
- 4. Half the original enzyme loading (5 FPU/50 units)

#### Results:

Established Steady States : The first run with com fiber and Labatt 1400 yeast in the continuous system was very successful. The run lasted 940 hours, at which time it was deliberately shut down. Under all tested conditions, ethanol was produced, the pH remained constant without vessel pH control, the yeast maintained its population and the glucose remained low. See figure 3 "Continuous SSF". The weight of the overflow slurry was plotted over time, then the actual residence times were calculated based on the slope of the resulting regression lines. The first target was a three day residence time. The calculated value was 75 hours (3 days and 3 hours) for the first setting. The second target was 2 days. The calculated value was determined to be 56 hours or 2 days and 8 hours. Both calculations represent very tight

lines with r-squared values of 0.9974 and 0.9975. See figure 4 "Overflow Balance Data". The compositional analysis at the time of start-up, showed approximately 6% cellulose in the wet slurry. Based on this number the experiments targeted 10 FPU, 20 FPU and 5 FPU. More recent compositional analysis of the com fiber showed a different cellulose number and a different oligomeric number, changing the enzyme loadings. The actual enzyme loadings were 25 FPU/200 units, 50 FPU/400 units and 12.5 FPU/100 units.

A steady state was established under the first set of conditions, 75 hour residence time and 25 FPU/200 units of cellulase and amylase enzymes.

Decreased residence time to 2 days: The residence time was actually decreased to 2 days and 8 hours (56 hours). Ethanol concentration in the vessel remained constant, thus volumetric conversion of the substrate increased. This is also validated by the mass spectrophotometer data which shows a higher volumetric production of carbon dioxide. Flow of carbon dioxide averaged 25 cc/day with the 75 hour residence time and 42 cc/day with the 56 hour residence time. See figure 5 "Off Gas Measurements on Continuous SSF".

Doubled the enzyme: The dilution rate remained the same and the enzyme feed rate was increased to deliver double the amount of cellulase and amylase. At this higher loading of 50 FPU/400 units, ethanol production did increase. Averaged steady state ethanol concentration increased from 14.5 to 15.1 g/L. Unfortunately, both enzyme loadings are saturating and the increase simply represents the additional amounts of glucose and sucrose supplied unavoidable components of the enzyme preparations.

Halved the enzyme: At the time of the experiment, it was believed that the new operational condition was 5 FPU as the enzyme pump was lowered to deliver half the volume of enzyme deliver in batch and the first steady state. Instead, 12.5 FPUs of cellulase and 100 units of amylase were delivered based on the actual composition of the extruded corn fiber. There was a drop in the average steady state ethanol concentration from 15.2 to 12.9 g/L. Also the detected flow of ethanol in the gas phase decreased from 950 to 800 PPM/day. Microscopic observations of the SSF began to include a wide variety of yeast morphologies. No pseudohyphae were observed, however there were small and medium and large cells. A YPD plate of the SSF slurry showed 2 main colonies. With the specter of a possible yeast contaminant present with the Labatt 1400, it was decided to shut down the SSF. A 24 hour fermentation was conducted on D5A. Labatt 1400 and the culture from the ECF continuous. Cultures were grown in two flasks, one with YPD and the other with YPX. Ethanol production and growth only occurred on YPD. Dry cell weight for all three cultures were 3.8 g/L. Ethanol concentrations were also similar at 9.08, 9.14, and 8.36 g/L.

### Comparison of Steady States

	Average Ethanol (v/E)	Std dev Ethanol	Theoretical Yield (C6)	Hours of SSF	Kilograms of Spent Shary
3 day Res Time 25/200	14.4	0.47	76.7	237	3.53
2 day Res Time 19/100	14.4	0.58	77.0	167	3.55
Donble enzyme 20/208	15.2	0.40	81.0	168	2.81
Low enzyme 12.5/50	12.9	0.86	69.0	228	4.67

Also see Figure 6, "Trend Lines for Continuous SSF" to see a graphical representation of the four above steady states.

At the time of shut down, solids and liquids from the harvested vessel were analyzed by the CAT task. The mass balance Excel spreadsheet developed in the first com fiber study, "Preliminary Experiments", April 1995" was used to check the mass balance on this last sample from the continuous. Two separate scenarios were performed because the solids analysis from the material harvested had a very poor mass balance closure.

Mass Balance Scenario One: The analysis from the solids and liquids actually taken from the continuous vessel were used in the Excel sheet. The mass balance on the solid material is at 75-77%, in other words, 25% of the solid is not accounted for after determining glucose, xylose, galactose, arbinose, mannose, klason lignin, acid-soluble lignin and ash. The analysis was performed again on this solid. Both analyses produced similar poor closures. This analysis is #95-057. The excel sheet shows a conversion of 18.79% on the lignin. Ethanol yield is 32.68 grams per 100 grams of C6 sugars converted. Ethanol process yield is 51.1% of theoretical in the SSF unit operation. Cellulose conversion is at 95.7%. The overall carbon recovery is 89.76%. Again a significant portion of the six carbon sugars remain in the liquor as unconverted oligomers. See Figure 7 "SSF Carbon Balance: continuous SSF on 40% cat95-057".

Mass Balance Scenario Two: The analysis of the solid residue from the shake flask study had closed to 89%. The main difference is the higher reported lignin. The analysis from this solids was placed in the excel sheet. The lignin conversion improved from 18.79 to -2.86. The overall carbon recovery improves to 94.71%. Ethanol remains unchanged. See figure 8 "SSF Carbon Balance:continuous SSF on 40% cat95-020". Also see Appendix 2, "CAT Task reports".

#### Conclusions:

The first attempt at continuous fermentation of Com Fiber was very successful. The run lasted 940 hours at which time it was deliberately shut down. The feed concentration of Com Fiber was 40 % w/w. This was the maximum solids loading that the magnetic stir bar in the feed jar could tolerate. The following steady state conditions were tested: 25 FPU/200 units 75 hour residence time, 25 FPU/200 units 56 hour residence time, 50 FPU/400 units 56 hour residence time, 12.5 FPU/100 units 56 hour residence time. The percent theoretical ethanol yields based on total six carbon sugars were 77, 77, 81 and 69 respectively. Unfortunately the enzyme loadings actually used in the experiment were all saturating for this substrate and thus may explain the relatively small differences in ethanol yield of the various tested conditions.

Glucose levels remained under 2 g/L through out the entire 940 hour run. The pH remained stable without vessel pH control (extruded com fiber feed was adjusted to pH 5 with lime before autoclaving). The yeast maintained their population in the fermentor at the tested dilution rates of 0.013 and 0.017 h<sup>-1</sup> which correspond to residence times of 75 and 56 hours. Continuous inoculation was not needed.

Based on plate cell counts, at the end of the run, an equal number of foreign yeast accompanied the Labatt 1400 parent strain. No other organisms were observed on the plates or under the microscope through out the run. Despite the presence of 10 g/L free xylose during the SSF, bacteria or other xylose utilizing organisms were not detected at any time.

Figure 1 Schematic of the Continuous System

Figure 2 Calibration of the Slurry Valve

Figure 3 Continuous SSF

Figure 4 Overflow Balance Data

Figure 5 Off Gas Measurements on Continuous SSF

Figure 6 Trend Lines for Continuous SSF

Figure 7 SSF Carbon Balance CAT057

Figure 8 SSF Carbon Balance CAT020

Appendix 1 Rotameter flow conversion sheet

Appendix 2 CAT task reports

Appendix 3 HPLC chromatogram of a sample from the continuous run

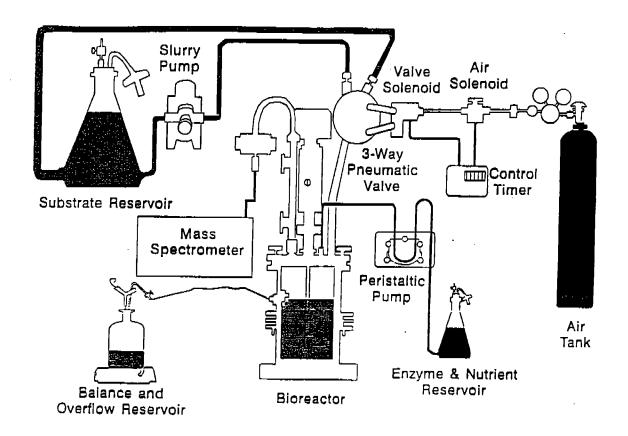
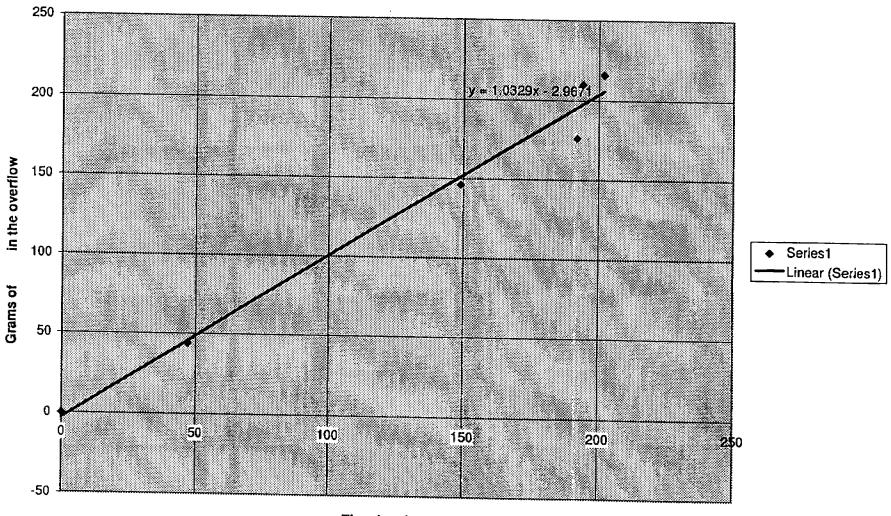


FIGURE 1. SCHEMATIC OF THE CONTINUOUS SSF SET-UP.

Calibration of Valve with pH 5

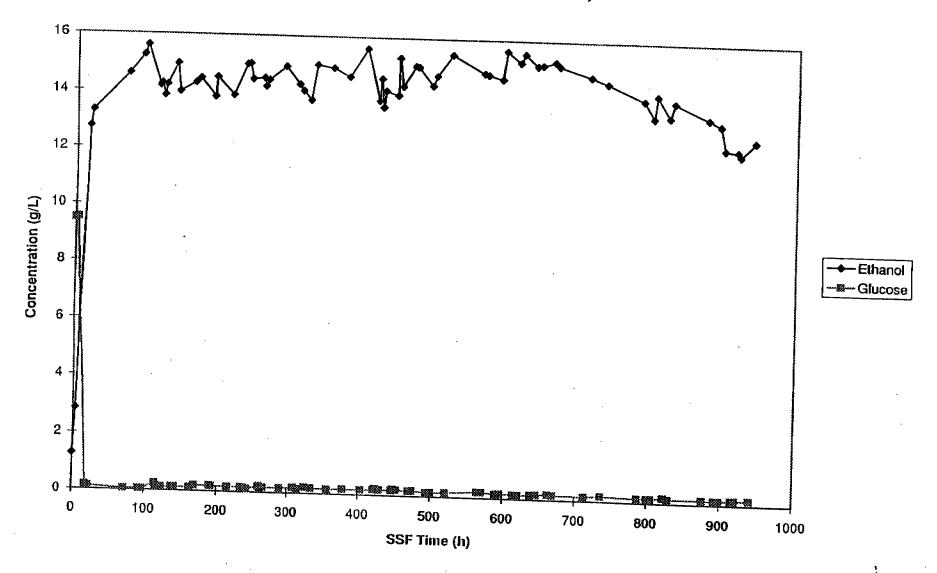


Time in minutes

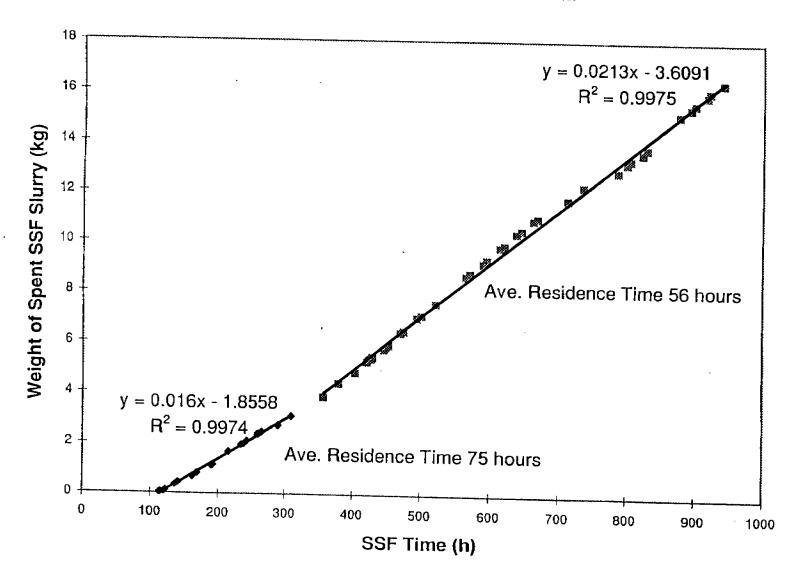
First run with

\*Corn Fiber, SSF ran in continuous mode for over 900 hours. Concentrations of glucose remain low. Ethanol levels are lower towards the end of the run when the enzyme loading was the lowest.

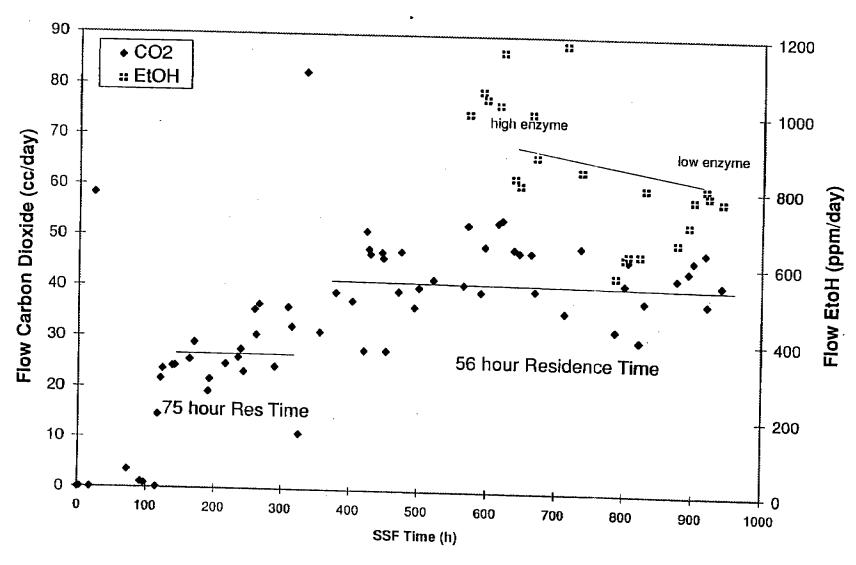
Continuous SSF with ECF run 18,1



### **Overflow Balance Data**

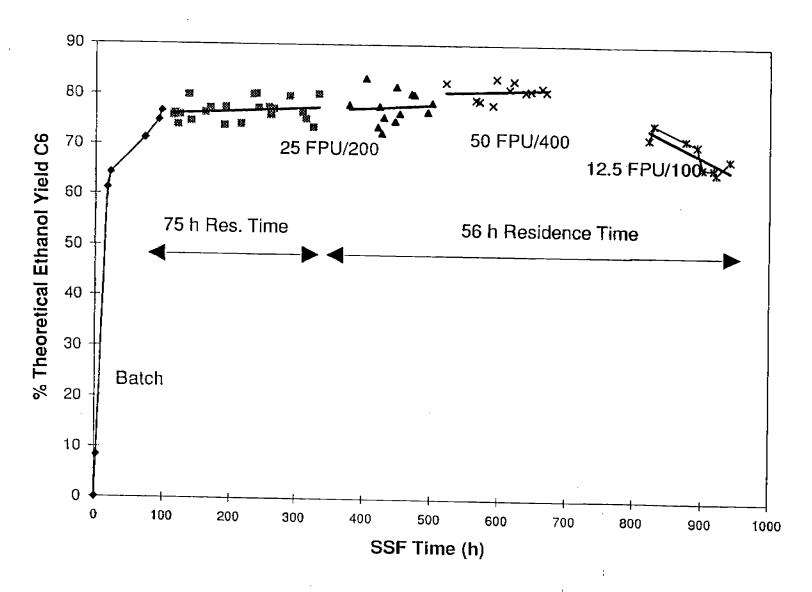


### Off Gas Measurements on Continuous SSF



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**Continuous SSF** 



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SSF CARBON BALANCE: (Continuous SSF on 40% Corn Fiber (cat95-057)

Sample; ; Prefreatment;

Run:

SOUDS BALANCE	kı	Out
Uguth (%):	30.83	54.0₹
Insoluble Solids (%):	3,50	1,40

Cellulose Conversion: 95.7%
Overall Cossugar Conversion: 80.0%
Overall Cossugar Conversion: 5,0%
Ethana Process Yield (% theor): 51.1%
Ethana Metabora Yield (% theor): 53.0%

Carbon Balance: SSF

_				arbon in				Carbon Out								
Component	in Solids (% dry wt) (C-mole/kg Si (% Total in)			In Liquor Fotal (g/L) (C-mole/Kg SII (% Total In) (C-mole/Kg SII)			In Solids (% dry wl) (C-mole/Kg Sir. Total Out)		in Liquer Total (g/L) (C-mole/kg six Total Out) (C-mole/kg Six				Conversion (in-Out)/in (%)			
Cellablase Glucase Glucase Galacitase Mannose Xylose Arabinose Lignin  Ethanol Cell Mass Carbon Dioxide Glycerol Acetic Acid Lactic Acid Succinic Acid	51.27 1.42 0.12 9.02 4.54 30.83	0,598 0.017 0.001 0.105 0.053 0.514	50,7 11.1 1.7 14.7 12.2 65.4	0.00 18.05 4.12 2.55 19.04 11.80 5.93 1.00 0.20 0.08 1.61 0.49 0.84	0.000 0.580 0.133 0.082 0.612 0.379 0.273 0.042 0.008 0.002 0.052 0.016 0.027	49.3 88.9 98.3 85.3 87.8 34.6	0.000 1.178 0.149 0.083 0.717 0.432 0.789 0.042 0.008 0.002 0.052 0.016 0.027	5.51 0.19 0.57 0.89 0.27 54.08	0.026 0.001 0.003 0.004 0.00)	13.7 1.0 100.0 0.6 0.3 56.5	0.00 4.91 2.61 0.00 20.39 12.35 5.92 12.20 2.24 0.55 3.02 2.92 1.68	0.000 0.161 0.092 0.000 0.670 0.408 0.279 0.522 0.088 0.254 0.018 0.099 0.096	86.3 99.0 0.0 99.4 99.7 43.5	0.600 0.187 0.093 0.674 0.407 0.641 0.522 0.088 0.254 0.018 0.099 0.096	84.13 37.51 96.81 6.06 5.87	32.68 5.95 33.08 1.39 4.20 7.10 2.50
Total	90.29	1.289	36.9		2.206	63.1	3,496	60.74	0.396	12.6		2.741	87.4	3.138		86,90

C-<del>ASCO</del>LBIN 89.76%

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### SSF CARBON BALANCE: (Continuous SSF on 40% Cosh Fiber (cal95-020)

Sample: Prefreatment: Run:

SOUDS BALANCE	lı	Out
Ugriin (∿):	30.83	79.61
insolutio Solida (%):	3,50	1.40

	######################################
Calluose Conversion: 96.5%	
Overall C& Sugar Conversion: 80.4%	
Overall C5-Sugar Conversion: 5,2%	
Ethanol Process Yield (% lineor): 51 1%	
Ethanal Metabolic yield (% Il rean) 63 a%	

### Carbon Balance: SSF

			c	arbon in				Carbon Oul								
Component	In Solids (% dry wl) (C-mole/kg str (% lotation)			in Liquor Total (g/L) (C-mole/Ky St (% Total In) (C-mole/Ky Sin)		In Solids (% day wit) (C-mole/Kg sha tole#On)						Total ∹nole(Kg St				
Cellobjose Glucose Glucose Galaciose Mannose Xylose Arabinose Lignin Ethänol Cell Mass Carbon Dioxida Glycerol Acello Acid Lactic Acid Succinic Acid	\$1.27 1.42 0.12 9.02 4.54 30.83	0.598 0.017 0.001 0.105 0.053	50.7 11.1 1.7 14.7 12.2 65.4	0.00 18.05 4.12 2.55 19.04 11.80 5.93 1.00 0.20 0.08 1.61 0.49 0.84	0.000 0.580 0.133 0.082 0.612 0.379 0.273 0.042 0.008 0.002 0.052 0.016 0.027	49.3 88.9 98.3 85.3 87.8 34.6	0.000 1.178 0.149 0.083 0.717 0.432 0.789 0.042 0.008 0.002 0.052 0.016 0.027	4.43 0.54 0.00 2.43 0.55 79.61	0.021 0.003 0,000 0.011 0.003	11.4 2.7 #DIV/OI 1.7 0.6 65.6	0.00 4.91 2.81 0.00 20.39 12.35 5.92 12.20 2.24 0.55 3.02 2.92 1.68	0.000 0.161 0.092 0.000 0.670 0.406 0.279 0.522 0.088 0.254 0.018 0.099 0.096	88.6 97.3 #DIV/OI 98.3 99.4 34.4	0.000 0.182 0.095 0.000 0.681 0.408 0.812 0.522 0.088 0.254 0.018 0.099 0.096	84.56 36.42 100.00 5.06 5.56 -2.86	32.51 5.92 32.90 1.38 4.18 7.06 2.49
Tolal	90.29	1.289	36.9		2.206	63.1	3,496	86.71	0.570	17.2		2.741	82,8	3.311		86.44

C-RECOVERY 94.71%

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SSF Carban Halance

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Material Company

Page 1

#### CHEMICAL ANALYSIS & TESTING Analysis Page No. 1 of 1 (CAT) Task Analytical Report 95-057 ject Title: Continuous SSF (ET60) NREL In-House Current Subcontractor CRADA Other X Name of Project Contact Person: Tammy Kay Hayward Date Work Completed: Revised report issued 5/18/95 NREL Notebook: 1561, p037 Date Samples Delivered: 3/17/95 Samples from Feedstock Lot No.: N/A Actual Hours Spent: 2 Summary of Requested Work: Complete compositional Proposed Approach: Standard LAPs by validated outside analysis. laboratory. Sample Prep Acid Digest **HPLC** YSI GCOther: Work Required: Results and Comments ☐ % As Received $\square$ % Dry Weight mg/mL Other: Sample G A M LKL LAS ΑT MB Continuous Final Pt. Autoclaved 35.11 15.67 2.53 ave 0.56 0.77 1.62 48.74 2.07 75.12 washed solids, 95-057-644, initial (March) analysis sd 0.12 0.57 0.00 0.08 0.02 0.10 0.87 0.09 0.01 Continuous Final Pt, Autoclaved 35.16 17.59 1.49 2.82 0.57 0.92 48.64 5.35 2.12 77.09 washed solids, 95-057-644. sd 0.21 0.22 reanalyzed (Mav) 0.10 0.02 0.02 0.05 0.16 0.12 0.02 ave sd ave sd ave sd sd A=arabinose; AC=acetic acid; AT=total ash; ET=ethanol; FA=formic acid; FL=furfural; G=glucose; G-YSI=glucose by YSI; GA=galactose: GLY=glycerol; HMF=5-hydroxymethyl-2-furaldehyde: LA=lactic acid: LAS=acid soluble lignin; LKL=Klason lignin: M=mannose; MB=mass balance. [(G+GA+M)x0.90 + (X+A)x0.88 +LKL + LAS + AT]; n/a=not applicable; nd=not detected; nr=not requested; P=protein: SA=succinic acid; TS=total solids; TDS=total dissolved solids; X=xylose; \*=Not enough sample to run in duplicate.

CC: Christos Hatzis

Love Brown

Name(s) of CAT Staff Working on Project: Larry Brown

Tina Shamay 5-19-95

Reviewed by: Tina Ehrman

# CHEMICAL ANALYSIS & TESTING (CAT) Task Analytical Penart

Analysis No. 95-020

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	CF1 (E	T60)	_		_							
NREL In-House Current Subcontra	ıctor	CRAD.	,	Other		Date Samples Delivered: 2/9/95						
						Date	Work	Promis	ed: 2/14	1/95		
Name of Project Contact Person: Tammy	Name of Project Contact Person: Tammy Kay Hayward						d: 2/	15/95		•		
NREL Notebook: #1561, p017, #1382, p1	108		Est	imated I	Iour	s Requ	uired:	4				
Samples from Feedstock Lot No.: n/a			Act	ual Hou	rs Si	ent:	4					
Summary of Requested Work: Complete analysis, protein content.	composi	tional		posed A pratory, j								
Work Required:	DF/ADF	Acid	Digest	_	.c X	YS	I ]	GC	Other			
Results and Comments	ived		× % 1	Ory Wei	ght			Oth	ier_7	٦.61		
Sample	TS	G	_ x	GA.	در		M	LKL	LAS	AT	MB	
1 Autoclaved SSF solid residue ave	30.60	4.43	2.43	0_54	0.5	55	0.0	73.80	5.81	1.53	89.09	
sd	0.21	0.33	0.11	0.02	0.0	7	0.0	0.29	0.23	0.03		
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sd	<del> </del>	<u> </u>			_							
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A=arabinose; AC=acetate: AD=detergent ash; A GA=galactose: H=mass % hydrogen; HC=h M=mannose; N=mass % nitrogen; nd=not det *=cal	emicellul tected; nu culated f	lose; L=d =not requirements	etergent uested: I gen me:	lignin; L protein=	AS= ; TS= · CH	acid so =total s N	oluble solids:	lignin; I UA≔uro	KT = K1	son ligni	in· I	

Tina Ehrman

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ct Title: Continuous SSF (ETc	50)				<u></u>	<u> </u>	<u> </u>		<u> </u>	<u> </u>		L		
NREL In-House	Current Subcontra							factor CRADA						
Name of Project Contact Person: Ta	Date	Work	Comp	leted:	3/31/95									
NREL Notebook: 1561 p 038, #138	Date Work Completed: 3/31/95  Date Samples Delivered: 3/17/95													
Samples from Feedstock Lot No.: N	/A			T	al Hou			3,11,5	<del>-</del>					
Summary of Requested Work: Mono sample as received organic acids, HA sample as received; total sugars in sa hydrolysis	Æ furðu	cal etha	nol in	Рторо	sed A	pproac	h: Star	ndard L e analy	APs by	y valida	ned ou	ıtside		
Work Required:	Acid I	Digest	HPL	.c ₹]	YSI	G	C 01	her:						
Results and Comments	Received G	x	% Dry GA	Weight A	X M	mg/u	nL LA	GLY	ther: AC	EMF	FL	ET		
Continuous final pt filter sterile averaged	e 1.53	10.94	1.65	9.13	0.00	1.68	2.92	0.55	3.02	0.00	0.07	12.2		
Sc	0.02	0.06	0.02	0.06	0.00	0.01	0.03	0.01	0.03	0.00	0.01			
95-058-645, after 4% acid ave hydrolysis	4.91	20.39	2.31	12.35	0.00		_			_				
sd	0.00	0.00	0.00	10.0	0.00	-	_	_		_	_			
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A=arabinose; AC=acetic acid: AT=total A=galactose; GLY=glycerol: HMF=5-hydr M=mannose; n/a=not applicable; nd=not dissolved sol	detected; ids; X=xy	nr=not r lose; *=1	equeste Not enc	d: P=nm	nein. 2	: LAS= 1-mcc	acid so	luble lig	YSI=gli nin; Lk val soli	ucose by CL=Klas	YSI; son lign s=total	rin:		
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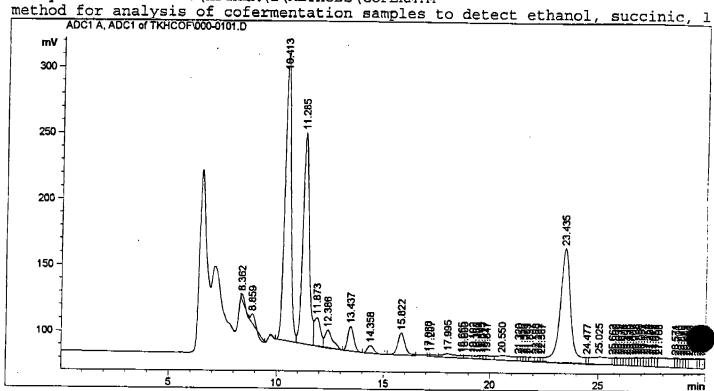
Sample Name: #49

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Acq Method : COFERM.M Seq. Line : Acq. Operator : KENT Vial :

Injection Date : 3/2/95 4:40:27 PM Inj : 1 Sample Name : #49 Inj Volume : 10  $\mu$ l

Sequence File : C:\HPCHEM\1\SEQUENCE\TKHCOF.S Analysis Method : C:\HPCHEM\1\METHODS\COFERM.M



### External Standard Report

Sorted by Signal

Calib. Data Modified : Thursday, March 02, 1995 12:29:20 PM

Multiplier : 1.000000 RF Uncal. Peaks : 1.000000

Signal 1: ADC1 A, ADC1

RT [min]	Туре	Area	Amt/Area	Amount (	Grp	Name
7 070	<del>-</del>		<del></del>		-	
7.872	*	not found	*		С	ellobiose
8.362	BV	48.62407	1.00000	48.62407	?	•
8.859	PV	58.57494	1.00000	58.57494	?	
9.750	*	not found	*		g	lucose
10.413	BV	4291.61719	2.32417e-3	9.97445	x	ylose
11.285	VV	3324.44800	1.00000	3324.44800	?	-
11.873	VV	440.38184	1.00000	440.38184	?	
12.386	VV	338.45407	2.72906e-3	9.23662e-1	s	uccinic acid
13.437	PV	377.72403	2.88063e-3	1.0880		- 04.d
14.358	PV	125.52240	3.34008e-3	4.19255e-L		
15.822	$\mathbf{VV}_{-}$	413-54282-	4.99691e-3	2.06643	a	cetic acid

	RT nin]	Туре	Area	Amt/Area	Amount [g/L]	Grp	Name
17.	080	) <b>V</b> V	10.34459	1.00000	10.34459	-	
		VV	32.14430				
17.	995	vv :	136.28113			_	
18.	665	VV	16.45382				
18.	800	VV	50.93551				
		VV .	17.61430	1.00000	17.61430		
		VV	18.48275		18.48275		
		VV	16.61640	1.00000	16.61640		
		VV	20.87583	1.00000	20.87583		
		VV	22.68722	1.00000	22.68722	?	
		VV	62.83945	1.00000	62.83945		
		VV	195.95222	1.00000	195.95222		
	320 <b>45</b> 6	VV	24.77899	1.00000	24.77899		
	430 576		24.07818	1.00000	24.07818	?	•
			27.12610	1.00000	27.12610	?	
	837		25.96850 55.04248	1.00000	25.96850	?	
	108		28,25650	1.00000	·	?	
22.			28.97863	1.00000		?	
22.			29.64168	1.00000	28.97863 29.64168	. Š.	
23.			2993.80420	5.59723e-3	16.75701	•	hanol
24.			40,17390	1.00000	40.17390	?	Inanor
25.	025	VV	354.63028	1.00000	354.63028	3	
25.	662	VV	39.16637	1.00000	39.16637	;	
25.	802	VV	42.83253	1.00000	42.83253	?	
25.			46.90511	1.00000	46.90511	?	
26.0			46.01423	1.00000	46.01423	?	
26.2			46.87158	1.00000	46.87158	?	
26.:			47.70601	1.00000	47.70601	?	
26.4			48.64779	1.00000	48.64779	?	
26.6			49.64444	1.00000	49.64444	?	
26.7			50.64853	1.00000	50.64853	?	
26.8			51.55343	1.00000	51.55343	3	
26.9 27.1			52.29885	1.00000	52.29885	?	
27.2			48.19789 52.51472	1.00000	48.19789	?	
27.3			53.71774	1.00000 1.00000	52.51472	3	
27.5			52.57881	1.00000	53.71774 52.57881	í	
27.6			53.60887	1.00000	53.60887	'n	
27.7			335.41895	1.00000	335.41895	,	
28.5			55.85745	1.00000	55.85745	2	
28.7	06	VV	50.86274	1.00000	50.86274	?	
28.8			55.35005	1.00000	55.35005	?	
28.9			56.70454	1.00000	56.70454		
29.1		VV	56.90847	1.00000	56.90847	?	
29.2		VV	174.96999	1.00000	174.96999		
29.6		VV	58.90648	1.00000	58.90648	?	
29.7			59.47293	1.00000	59.47293	?	
29.8	<b>J</b> /	VBA	33.00539	1.00000	33.00539	3	•
rot = 1					5063 ED445		

Totals :

6863.52441

1 Warnings or Errors :

Warning : Calibrated compound(s) not found